

# A/C Model Development and Validation













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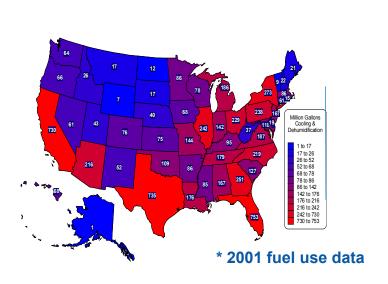
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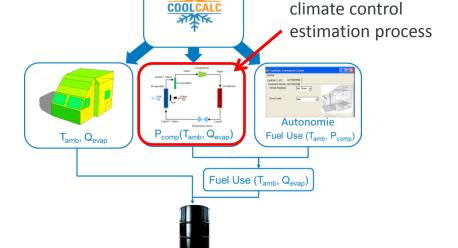
**Project ID VSS120** 

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# **Background**

- When operated, the air conditioning (A/C) system is the largest auxiliary load
- A/C loads account for more than 5% of the fuel used annually for light-duty vehicles (LDVs) in the United States<sup>1</sup>
- A/C load can have a significant impact on electric vehicle (EV), plug-in hybrid electric vehicle, and hybrid electric vehicle performance
  - Mitsubishi reports that the range of the i-MiEV can be reduced by as much as 50% on the Japan 10–15 cycle when the A/C is operating<sup>2</sup>
  - Hybrid vehicles have 22% lower fuel economy with the A/C on<sup>3</sup>
- Increased cooling demands by an EV may impact the A/C system
- A/C contributes to heavy-duty vehicle idle and down-the-road fuel use





Fuel Use Rate

Integral part of

improved high-level

<sup>1.</sup> Rugh et al., 2004, Earth Technologies Forum/Mobile Air Conditioning Summit

<sup>2.</sup> Umezu et al., 2010, SAE Automotive Refrigerant & System Efficiency Symposium

<sup>3.</sup> Idaho National Laboratory, Vehicle Technologies Program 2007 annual report, p145.

# **Overview**

#### **Timeline**

**Project Start Date: FY11** 

**Project End Date: FY13** 

**Percent Complete: 80%** 

### **Budget**

**Total Project Funding:** 

DOE Share: \$900K

Contractor Share: \$0k

**Funding Received in FY12: \$300K** 

**Funding for FY13: \$300K** 

#### **Barriers**

- Cost Timely evaluation of HVAC systems to assist with R&D
- Computational models, design and simulation methodologies – Develop tool to help with optimization of future HVAC designs and prediction of impacts on fuel economy
- Constant advances in technology Assist industry advance technology with improved tools

#### **Partners**

- Collaborations
  - Halla Visteon Climate Control (Visteon)
  - Argonne National Laboratory (ANL)
  - Daimler Trucks
- Project lead: NREL

# Relevance/Objectives

# Overall Objectives

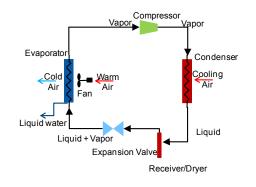
- Develop analysis tools to assess the impact of technologies that reduce the thermal load, improve the climate control efficiency, and reduce vehicle fuel consumption
- Develop an open source, accurate, and transient A/C model using the
   Matlab/Simulink environment for co-simulation with Autonomie
- Connect climate control, cabin thermal, and vehicle-level models to assess the impacts of advanced thermal management technologies on fuel use and range

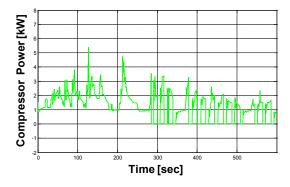
# FY12/13 Objectives

- Improve mechanical LDV A/C model and validate
- Add electrical compressor capability and associated controls
- Develop simplified model options for more rapid, less detailed analysis,
   with a focus on vehicle co-simulation with Autonomie
- Demonstrate co-simulation of A/C system with Autonomie
- Develop heavy-duty vehicle sleeper and cab A/C system models
- Release A/C model plug-in for Autonomie

# Milestones, FY12-FY13

Date	Milestone or Go/No-Go Decision		
04/01/2012	Delivered stand-alone model to Visteon		
06/14/2012	Delivered electric A/C model to ANL		
06/01/2012	Completed initial validation		
09/30/2012	Completed summary report and first release of the A/C model		
04/15/2013	Autonomie integrated model released		
04/16/2013	SAE World Congress paper "A New Automotive Air Conditioning System Simulation Tool Developed in MATLAB/Simulink," SAE 2013-01-0850		
09/30/2013	Summary report and second release of the A/C model		







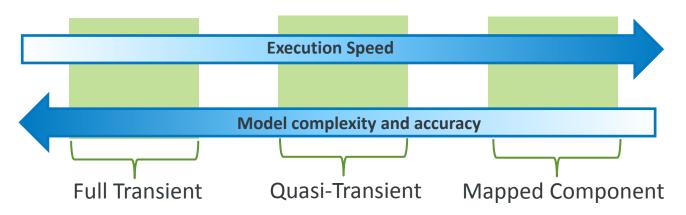
# **Approach – Matlab/Simulink-Based Tool**

- Base a simulation tool on first principles; conservation of mass, momentum, and energy are solved in 1-D finite volume formulation
- Create open source software tools and make them available to the public
- Easily interface to Autonomie vehicle simulation tool
- Develop flexible software platform, capable of modeling vapor compression refrigeration cycle
- Model refrigerant lines and the heat exchangers as 1-D finite volumes, accounting for the lengthwise distribution of refrigerant and flow properties
- Include all major components: compressor, condenser, expansion device, evaporator, and accumulator/dryer (receiver/dryer)
- Provide model options with a range of run times while minimizing the impact of increasing speed on accuracy to meet a range of analysis needs

# **Approach: Three Model Versions**

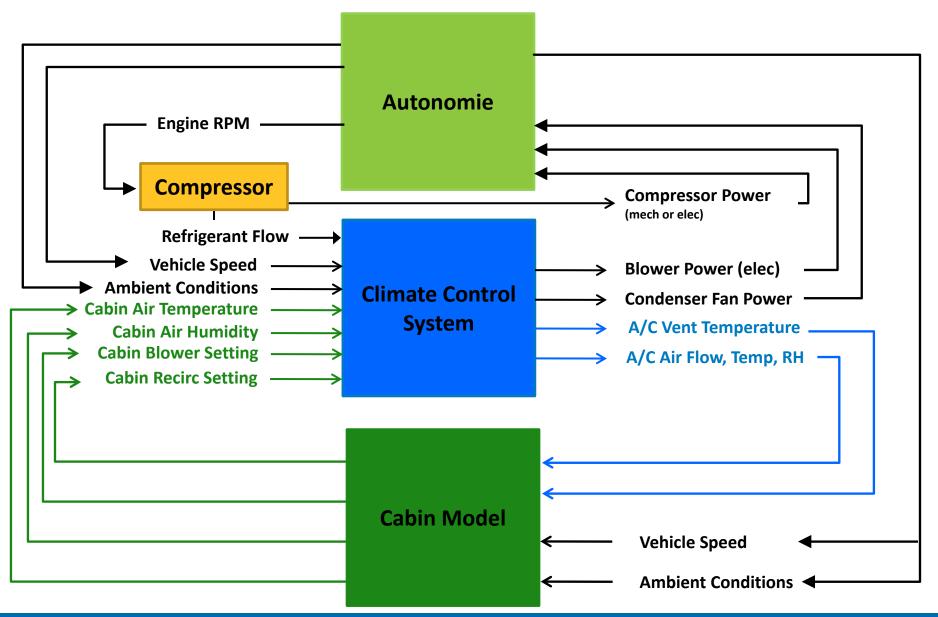
### Serving Different Customer Needs

Model Type	Application	Speed	Accuracy
Full Transient (finite volume, fully conservative)	Detailed A/C models for design and control	1/12th of real time	Highest, time- resolved
Quasi-Transient (simplified refrigerant volumes)	Detailed vehicle co- simulation and created mapped components	Real time	Moderate
Mapped Component (simplified refrigerant volumes and heat exchangers)	High level co-simulation with a vehicle focus	10 X real time (estimated)	Lowest



### **Approach: Climate Control System Integration with Autonomie**

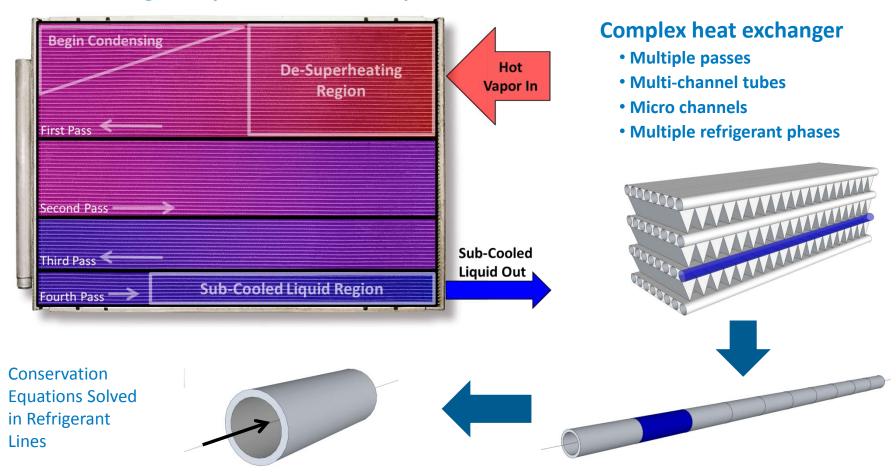
Enables co-simulation with vehicle models



# **A/C Model Development**

## Development of Component Models, Heat Exchanger

#### Four refrigerant passes in this example



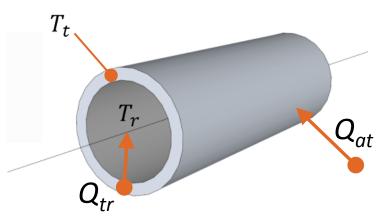
- Four refrigerant passes become four flow paths in this example
- Each flow path is divided into many segments, or finite volumes
- The 1-D finite volumes account for the lengthwise distribution of refrigerant and flow properties

### **Accomplishments: Heat Transfer**

#### Improved heat transfer and fin heat loss calculations

#### Pipe wall to refrigerant

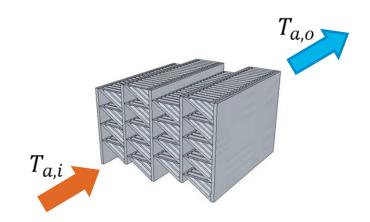
$$Q_{tr} = \overline{h}_{tr} A_t (T_t - T_r)$$



#### Heat transfer from air to pipe wall<sup>3</sup>

$$Q_{at} = \left(\dot{m}_a \cdot C_{p,adry} + \dot{m}_w \cdot C_{p,w}\right) \cdot \left(T_{a,o} - T_{a,i}\right)$$

$$T_{a,o} = T_{a,i} + \left(T_t - T_{a,i}\right) \cdot \left[1 - \exp\left(\frac{-\bar{h}_a A}{\dot{m}_a \cdot \left(C_{p,adry} + \omega C_{p,w}\right)}\right)\right]$$



#### Calculation assumptions:

- h<sub>wr</sub> obtained from Dittus-Boelter equation and Chen correlation
- $h_a$  obtained through correlations for louver fin compact heat exchangers<sup>1,2</sup>
- Fin effectiveness calculated using Number of Transfer Units (NTU) method
- Pipe modeled as radially isothermal, contains thermal mass
- Saturated mixture refrigerant properties are quality averaged values of sat. liquid and sat. vapor
- System accounts for possible water condensation in the air stream

<sup>1.</sup> Chang, Y.J., and Wang, C.C., "A Generalized Heat Transfer Correlation for Louver Fin Geometry," Int. J. Heat Mass Transfer, Vol. 40, No. 3, pp. 533-544, 1997

<sup>2.</sup> Chen, J.C. (1966). "A Correlation for Boiling Heat Transfer of Saturated Fluids in Convective Flow," Ind. Eng. Chem. Process Ses. Dev., Vol. 5, No. 3, pp. 322-329.

<sup>3.</sup> See nomenclature slide at end of presentation

### **Accomplishments: Compressor**

#### Added electric compressor and associated controls

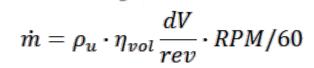
#### Compressor, general

Mechanical (piston) or electrical (scroll), electrical added this year

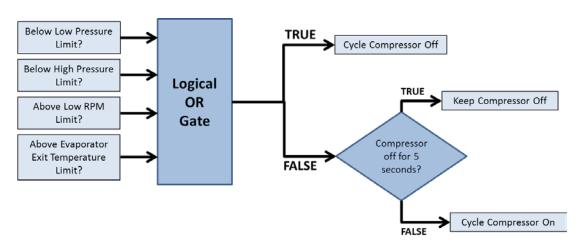
- Volumetric efficiency
- Discharge enthalpy found using isentropic efficiency

#### Electric compressor

- RPM controlled by T<sub>wall,evap,exit</sub> (metal T)
- Blower air mass flow rate controlled by T<sub>air,cabin</sub>
- No windup PI controllers implemented



 If compressor RPM command goes below limit, compressor cycles off. When compressor comes back, it starts up near this limit



[1] Compressor photograph, NREL, John Rugh & Jason Lustbader

[1]

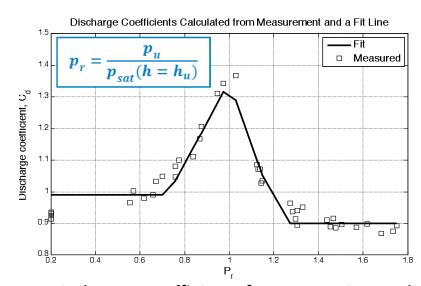
# **Accomplishments: Thermal Expansion Device (TXV)**

Semi-dynamic model improves TXV accuracy

#### Thermal Expansion Device (TXV)

- Two-phase equilibrium orifice flow model
- Capturing flow area dependence on evaporator-out superheat
- Semi-dynamic<sup>1</sup> model addresses response time issues
  - Valve ball position determined from static force balance
  - One dynamic factor bulb temperature response to evaporator exit temperature
  - Response is fast to pressure differences but slow to temperature changes – just like in a real TXV

$$\dot{m} = C_d(dP_e) \cdot \rho_{throat} \cdot v_{throat} \cdot A_{orif}$$



Discharge coefficient from experimental data accounts for non-equilibrium effects

<sup>&</sup>lt;sup>1</sup> This was found to have superior performance to a full dynamic model, which was also developed

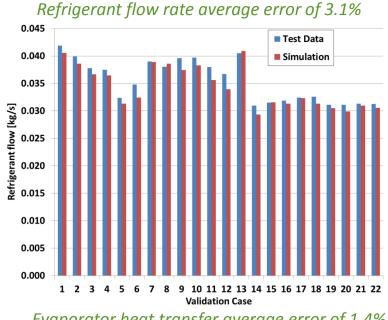
# **Accomplishments: Component Validation** *Validation data cover wide range of operating conditions*

- Model results compared to 22 steady-state experimental bench data points provided by Visteon
- Test points cover a wide range of operating conditions

Range of Bench Test Data						
	Low	High	Units			
Vehicle speed	0	112	km/h			
Ambient air temperature	21	43	°C			
Relative humidity	25	40	%			
Evaporator air inlet temperature	10	43	°C			
Evaporator air flow	0.042	0.137	m³/s			

#### **Accomplishment – Component Validation**

Improvements to model resulted in better agreement with data



Evaporator heat transfer average error of 1.4%

5.0

1.0

1.0

1.2

3.4

5.6

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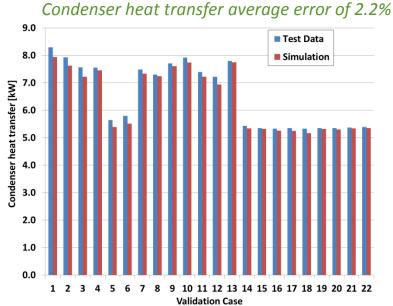
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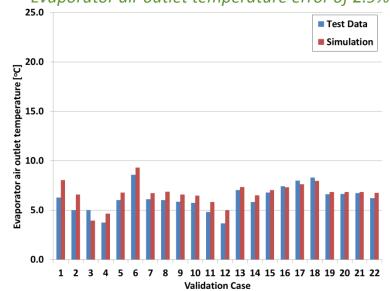
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Validation Case





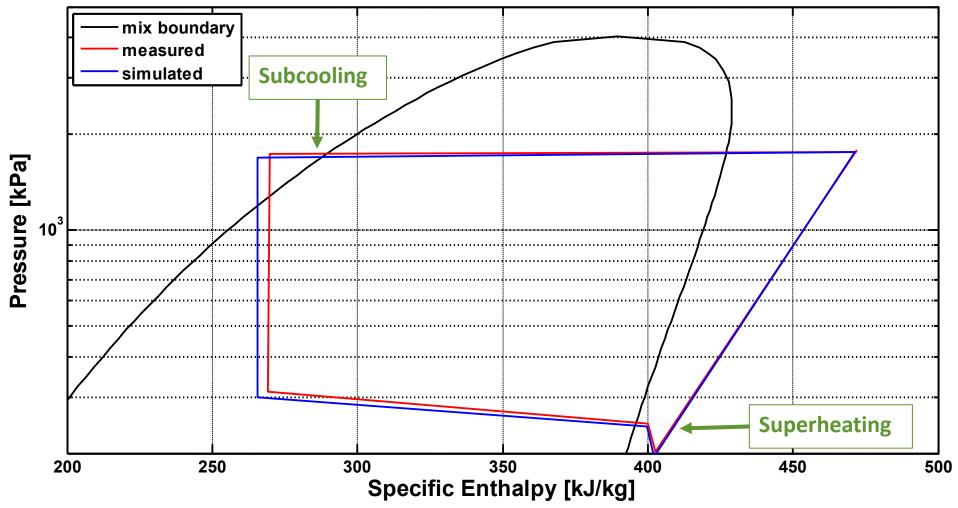


# **Accomplishment – System Validation, Typical Point**

Good Agreement for System Thermodynamic Cycle

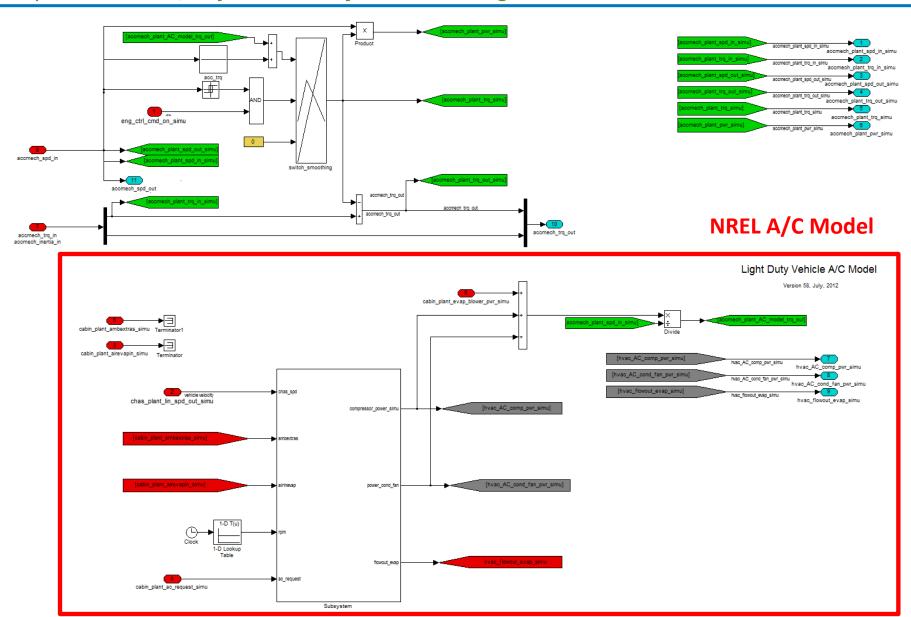
Full transient model





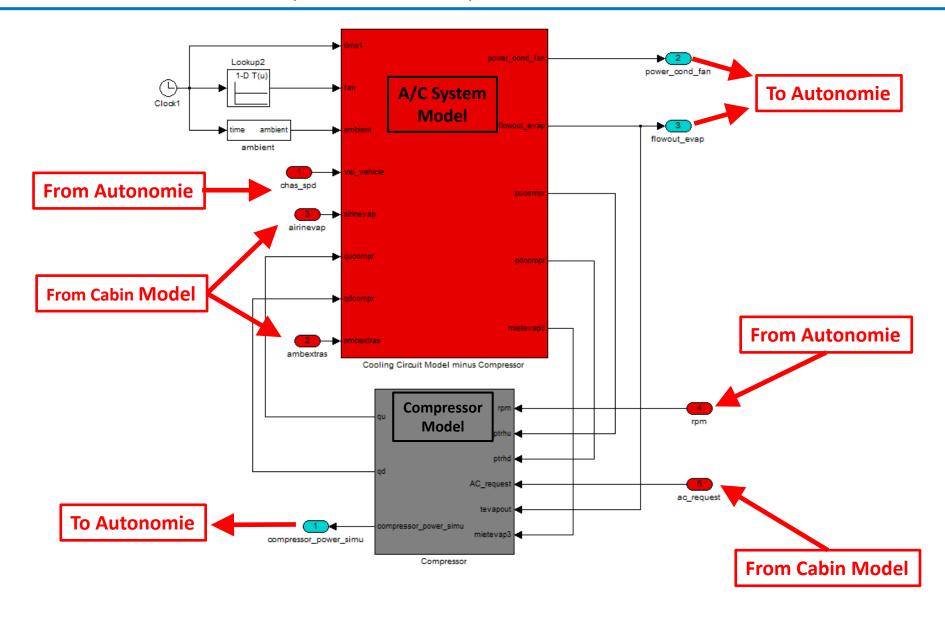
# **Accomplishments – Autonomie Integration**

Top-level model, adjusted code for better integration with next Autonomie release



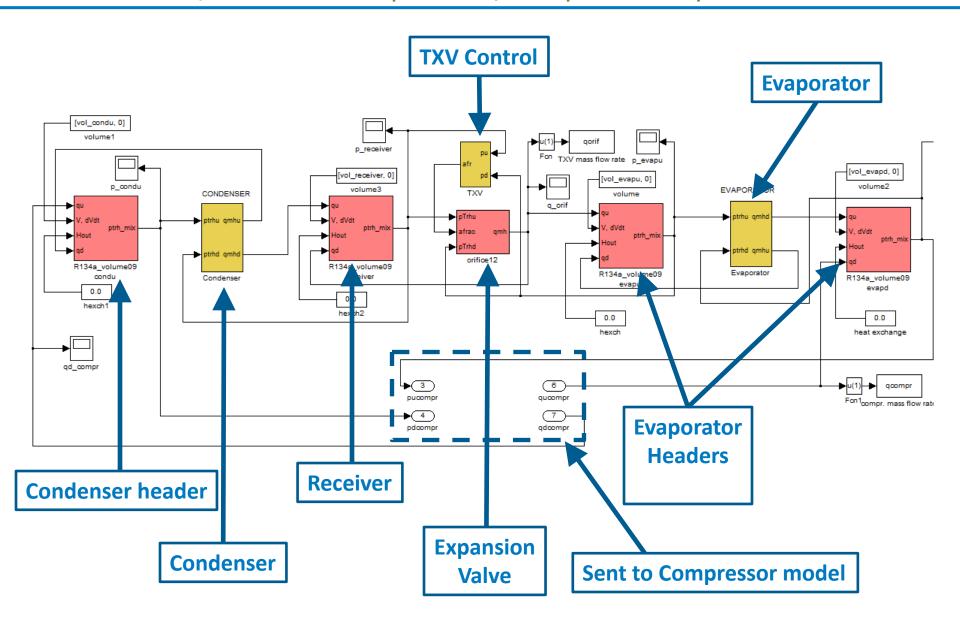
### **Accomplishments – Autonomie Integration**

Second-level model: Compressor made separate and cabin moved to chassis



# **Accomplishments – Autonomie Integration**

Third-level A/C model: Components, compressor separated



## **Accomplishments – SC03 Cycle**

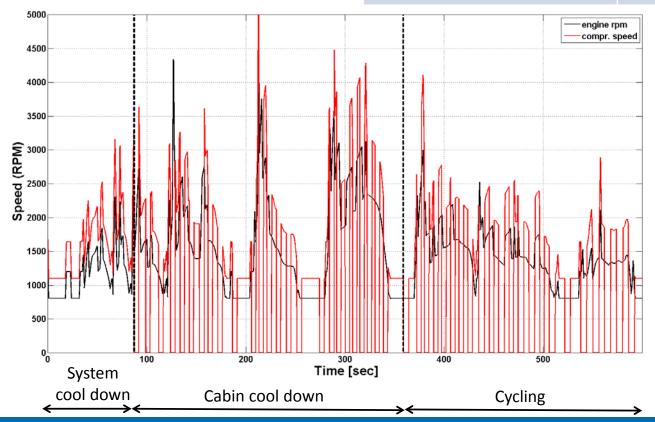
### System model SC03 example

# Simulated the A/C system over drive cycle

- Used SC03 drive cycle
- Conventional 2wd Midsize Auto Default in Autonomie
- Demonstrated robust system performance and cabin cooldown

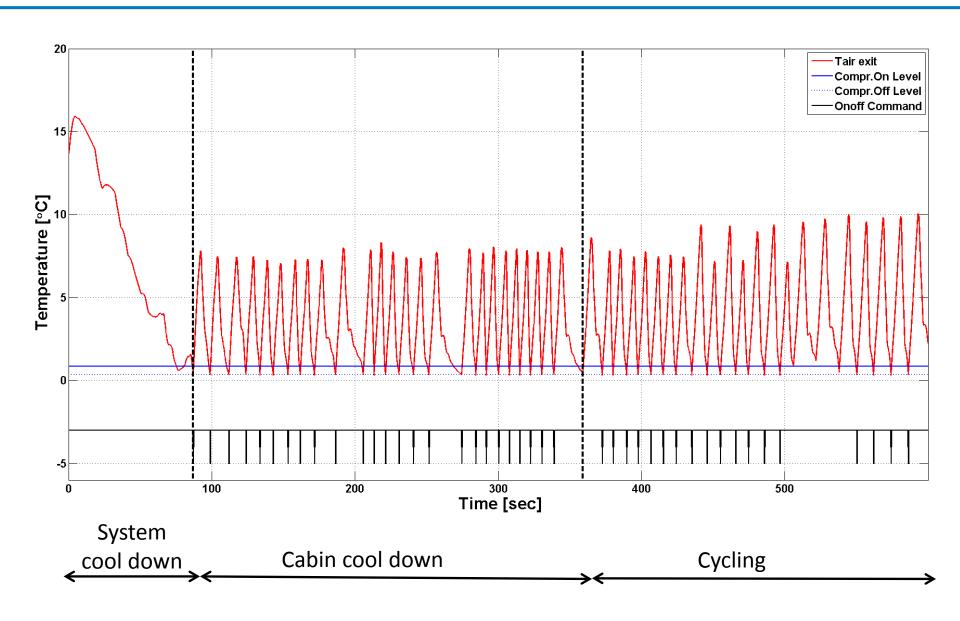
#### **Conditions and Controls Settings**

Variable	Value	Units
Ambient Temperature	30	°C
Cabin initial relative humidity	40	%
Solar load	1000	W
Cabin target temperature	20	°C
Air recirculation	90	%



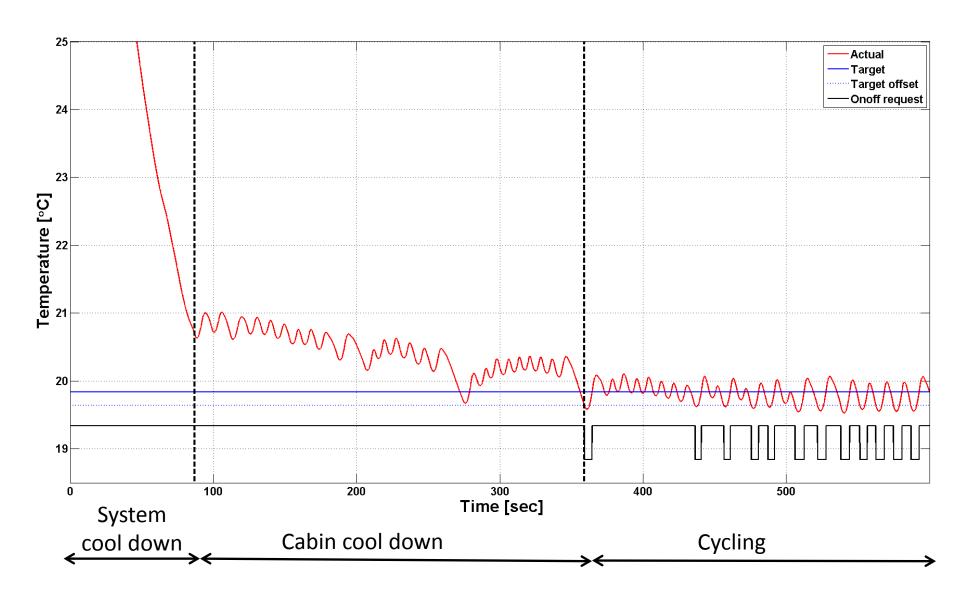
#### **Accomplishments – SC03 Cycle Evaporator Temperature Control**

Evaporator freeze protection control reached in 87 sec



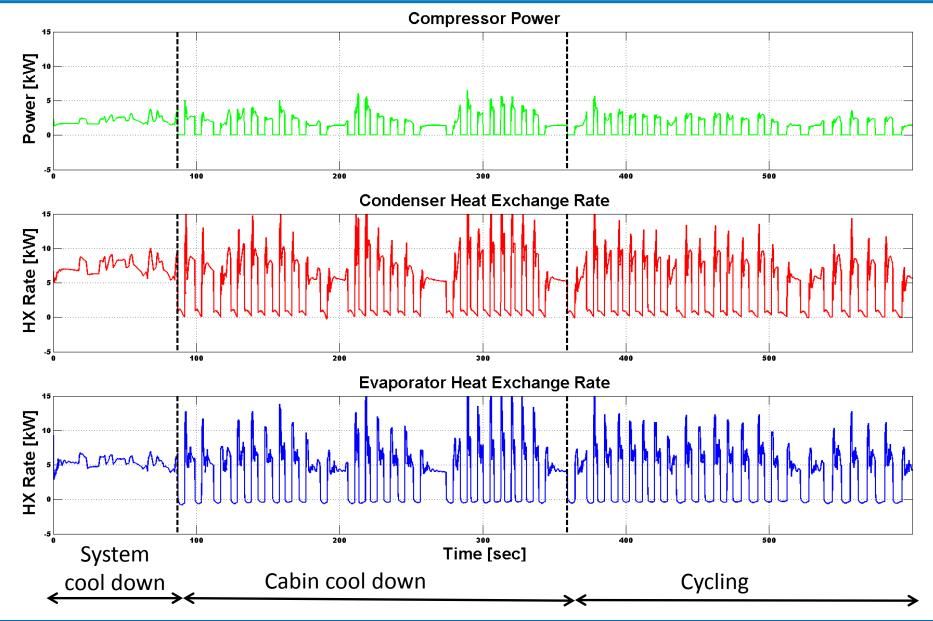
#### **Accomplishments – SC03 Cycle Cabin Temperature Control**

Cabin temperature control reaches set point in 359 sec



# **Accomplishments – SC03 Cycle Heat and Compressor Power**

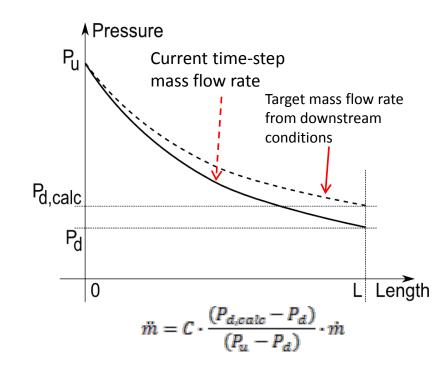
Dynamic thermal and mechanical power captured

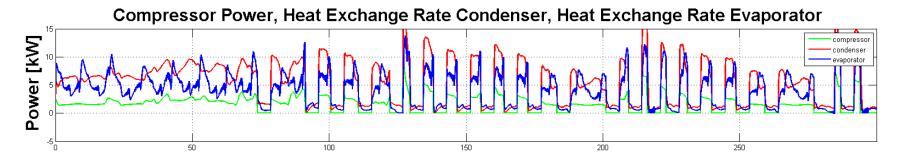


#### **Accomplishments – Quasi-Transient Model**

Simplifications to increase maximum time step and thus speed by 12X

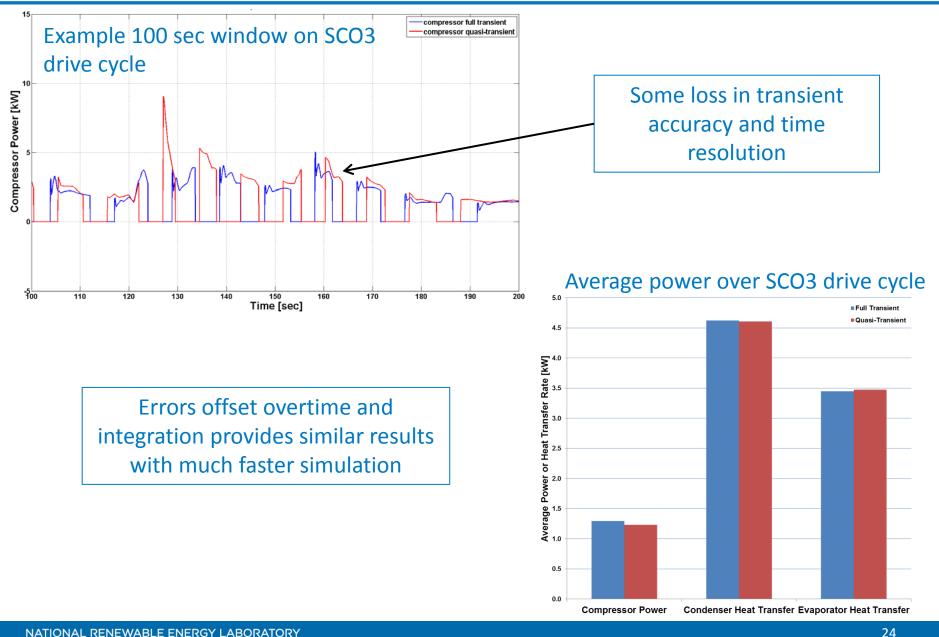
- Only refrigerant line and 0-D volume simulation blocks modified
- Modifications allow larger simulation time steps and thus faster execution speed
- Changes to refrigerant line blocks
  - Refrigerant side formulation no longer finite volume, algebraic marching scheme used
  - Mass flow rate
    - Same in all the segments of the line
    - Only state variable (calculated from its time derivative through an integration step)
  - Allows larger simulation time step
- Changes to 0-D volume blocks
  - Mass and energy are preserved
  - A modified bulk modulus is used (compressibility adjusted) to calculate the pressure in the volume
  - Allows for a larger time step





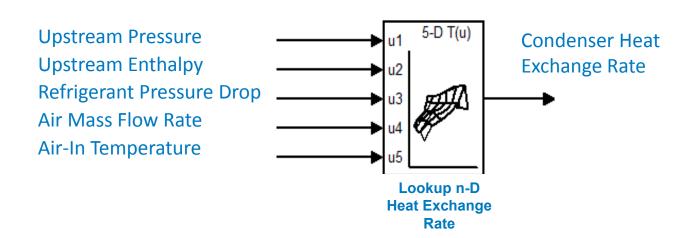
### **Accomplishment – Quasi-Transient Compared to Full Transient**

Good agreement between models over full cycle, quasi-transient 12 times faster



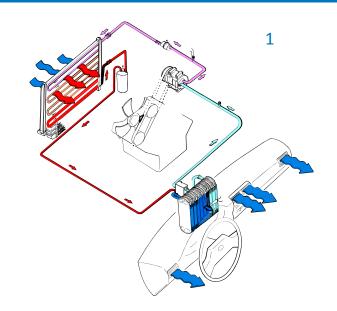
# Accomplishments – Mapped A/C Model development Faster execution time, ~10X real time (120 X Full Transient model)

- Heat exchanger calculations replaced by performance maps
- Quasi-transient model used to create lookup tables for the condenser and evaporator
  - 5- and 6-dimensional lookup tables are the best compromise between speed and accuracy, respectively
- Several thousand steady-state simulations were conducted for both condenser and evaporator to create the lookup tables
- Working on improving the model further



# **Collaboration**

- Halla Visteon Climate Control
  - Technical advice
  - A/C system and component test data
  - Co-authored paper for SAE
     World Congress
- Argonne National Laboratory
  - Integration of A/C model into Autonomie
  - Vehicle test data
- Daimler Trucks
  - Support Super Truck work



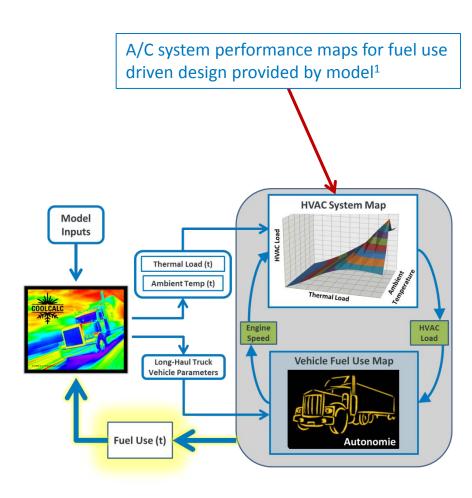


- 1. Diagram courtesy of Visteon Corporation
- 2. Daimler Super Truck Logo, Courtesy of Daimler Trucks, 2011

# **Future Work**

#### **FY13**

- Complete long-haul truck sleeper A/C system model for use with CoolCalc
- Validate model with ANL's
   Advanced Powertrain
   Research Facility (APRF) data
- Develop and release mapped component models (will run 10X real time) for cosimulation with Autonomie
- Release Autonomie A/C plug-in and updated standalone model



1. See VSS075, CoolCab Test and Evaluation & CoolCalc HVAC Tool Development presentation for more information

# **Summary**

#### **DOE Mission Support**

- A/C use can account for significant portion of the energy used by light-duty and heavy-duty vehicles.
- Reducing A/C energy use is essential to achieving the President's goal of 1 million electric drive vehicles by 2015.

#### **Approach**

- Develop a transient open source Matlab/Simulink-based HVAC model that is both flexible and accurate. Base model on first principles and do not rely on component flow and heat transfer data as input.
- Interface HVAC model with Autonomie vehicle simulation tool to simulate effects of HVAC use on vehicle efficiency and range.

# **Summary**

# **Technical Accomplishments**

- Improved a Matlab/Simulink model of light-duty vehicle A/C system and showed close agreement with experimental data over a wide range of operating conditions
- Added electrical compressor capability and associated controls
- Improved model for co-simulation with Autonomie
- Developed simplified model options for more rapid, less detailed analysis, with a focus on vehicle co-simulation with Autonomie
- Developed an initial heavy-duty vehicle sleeper system model
- Presented "A new Automotive Air Conditioning System Simulation Tool Developed in MATLAB/Simulink" at SAE world congress.

#### **Collaboration**

- Halla Visteon Climate Control
- Argonne National Laboratory
- Daimler Trucks

# **Summary – Acknowledgments**

- U.S. Department of Energy
  - Lee Slezak, Vehicle Technologies Program
  - David Anderson, Vehicle Technologies Program
- Halla Visteon Climate Control
  - John Meyer
- Argonne National Laboratory
  - Aymeric Rousseau

#### References

#### nomenclature

Q<sub>tr</sub> is heat transfer from pipe wall to refrigerant

h<sub>tr</sub> is the heat transfer coefficient from pipe wall to refrigerant

A, is the area of inner pipe surface

T<sub>t</sub> is the pipe wall temperature

T<sub>r</sub> is the refrigerant temperature

Q<sub>at</sub> is heat transfer from air to pipe wall

m<sub>a</sub> is mass flow of air

C<sub>p. adry</sub> is constant pressure specific heat of dry air

m<sub>w</sub> is the mass flow of water

C<sub>p,w</sub> is constant pressure specific heat of water vapor

T<sub>a o</sub> is air temperature out, or leaving

T<sub>a,i</sub> is air temperature in, or entering

h<sub>a</sub> is the heat transfer coefficient from air to pipe wall

A is the total heat transfer area

 $\omega$  is absolute humidity



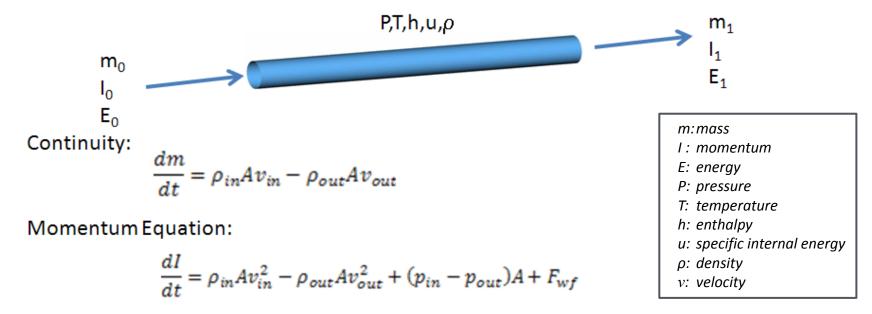
# **Technical Back-Up Slides**

# A/C Model Development

#### Development of Component Models, Line Segment

#### **Conservation Equations Solved in Refrigerant Lines**

(One-dimensional Finite Volume Formulation)



**Energy Equation:** 

$$\frac{dE}{dt} = Av_{in}\left(p_{in} + u_{in}\rho_{in} + \rho_{in}\frac{v_{in}^2}{2}\right) - Av_{out}\left(p_{out} + u_{out}\rho_{out} + \rho_{out}\frac{v_{out}^2}{2}\right) + Q_{tr}$$

where 'in' and 'out' subscripts mean inlet boundary and outlet boundary of finite volume, respectively

 $(F_{wf}$  is wall friction and  $Q_{tr}$  is heat addition rate)

Condenser wall to refrigerant:  $Q_{tr} = \overline{h}A_i(T_t - T)$ 

where the film coefficient is calculated with the Dittus-Boelter equation:

$$\left(\overline{Nu}_D \equiv\right) \frac{\overline{h}D}{k} = 0.023 Re_D^{4/5} Pr^n$$

The coefficient n can be modified for a particular geometry.

#### Evaporator wall to refrigerant: $Q_{tr} = h_{tp}A_i(T_t - T)$

where the film coefficient is calculated with the Chen correlation:

$$h_{tp} = h_{FZ}S + h_LF$$
 (composed of the sum of boiling and convective contribution)

h<sub>FZ</sub> is the Forster-Zuber correlation for nucleate boiling

$$h_{FZ} = 0.00122 \left[ \frac{k_L^{0.79} c_{pL}^{0.45} \rho_L^{0.49}}{\sigma^{0.5} \mu_L^{0.29} h_{LG}^{0.24} \rho_G^{0.24}} \right] \Delta T_{sat}^{0.24} \Delta P_{sat}^{0.75}$$

(h<sub>LG</sub> is the latent heat of vaporization, subscript L is liquid phase, subscript G is vapor phase,  $\Delta T_{sat}$  is the temperature difference between the inner tube wall [T<sub>wall</sub>] and local saturation temperature [T<sub>sat</sub>])

h<sub>L</sub> is the liquid phase heat transfer coefficient given by the Dittus-Boelter correlation

$$h_L = 0.023 Re_L^{0.8} Pr_L^{0.4} \left(\frac{k_L}{d_i}\right) \qquad Re_L = \frac{\dot{m}(1-x)d_i}{\mu_L} \qquad Pr_L = \frac{c_{pL} \mu_L}{k_L}$$

#### **Evaporator wall to refrigerant (continued):**

F is Chen's two-phase multiplier, and  $X_{tt}$  is the Martinelli parameter, which accounts for the two-phase effect on convection

$$F = \left(\frac{1}{X_{tt}} + 0.213\right)^{0.736} \quad X_{tt} = \left(\frac{1-x}{x}\right)^{0.9} \left(\frac{\rho_G}{\rho_L}\right)^{0.5} \left(\frac{\mu_L}{\mu_G}\right)^{0.1}$$

S is the Chen boiling suppression factor:

$$S = \frac{1}{\left(1 + 0.00000253Re_{tp}^{1.17}\right)} \qquad Re_{tp} = Re_{L}F^{1.25}$$

Chen, J.C. (1966). "A correlation for Boiling heat Transfer of Saturated Fluids in Convective Flow," *Ind. Eng. Chem. Process Ses. Dev.*, Vol. 5, No. 3, pp. 322-329.

#### Heat transfer from air to pipe wall:

$$Q_{at} = \overline{h}_a A_o (T_a - T_t)$$

 $j = 0.425 * Re_{Lp}^{-0.496}$  where j is the Colburn factor

j = St \* Pr
$$^{0.666}$$
 and  $St = \frac{h_a}{c_p \rho V}$ 

and Re<sub>Lp</sub> is the Reynolds number based on the louver pitch.

Or the more general correlation by Chang and Wang

$$j = Re_{Lp}^{-0.49} \left(\frac{\theta}{90}\right)^{0.27} \left(\frac{F_p}{L_p}\right)^{-0.14} \left(\frac{F_l}{L_p}\right)^{-0.29} \left(\frac{T_d}{T_p}\right)^{-0.23} \left(\frac{l}{L_p}\right)^{0.68} \left(\frac{T_p}{L_p}\right)^{-0.28} \left(\frac{\delta_f}{L_p}\right)^{-0.05}$$

Where  $\Theta$  is the louver angle,  $F_p$  is the fin pitch,  $L_p$  is the louver pitch,  $F_l$  is the fin length,  $L_l$  is the louver length,  $T_d$  is the tube depth,  $T_p$  is the tube pitch, and  $\delta_f$  is the fin thickness.

Chang, Y.J., and Wang, C.C., "A Generalized Heat Transfer Correlation for Louver Fin Geometry," *Int. J. Heat Mass Transfer*, Vol. 40, No. 3, pp. 533-544, 1997.

# A/C Model Development

#### Compressor Model

- Subscripts u and d are for upstream and downstream, respectively
- Mass flow rate:

$$\dot{m} = \rho_u \cdot \eta_{vol} \frac{dV}{rev} \cdot RPM/60$$

where  $\eta_{vol} = \eta_{vol}(\frac{p_d}{p_u},RPM)$  and dV/rev is the displacement per revolution

• Downstream enthalpy (h<sub>d,actual</sub>) calculated using isentropic efficiency:

$$h_{d,actual} = h_u + \frac{h_{d,isentropic} - h_u}{\eta_{isentropic}}$$

• where  $h_{d,isentropic} = h(s_u, p_d)$  and  $\eta_{isentropic} = \eta_{isentropic}(\frac{p_d}{p_u}, RPM)$ 

# **A/C Model Development**

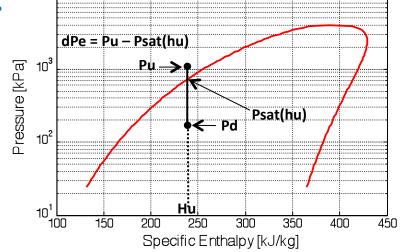
### Thermal Expansion Valve (TXV) Model

- Two-phase equilibrium orifice flow model with feedback control on orifice flow area based on Evaporator-out superheat ('SH')
- Orifice flow model calibrated to measured data using a discharge coefficient that is dependent on  $dP_{\rho}$  10<sup>t</sup>

$$\dot{m} = C_d(dP_e) \cdot \rho_{throat} \cdot v_{throat} \cdot A_{orif}$$

Feedback control:

$$\frac{dA_{orif}}{dt} = -C \cdot (T_{SHtarget} - T_{SH})$$



- Large C results in quick convergence but may lead to hunting
- Small C results in slow convergence but avoids hunting